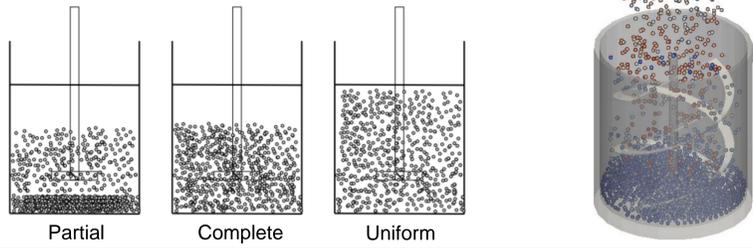


## SOLID-LIQUID MIXING

Multiphase mixing objective is to maximise contact between phases

The principal factor to characterize solid-liquid mixing is  $N_{js}$  : Just Suspended Speed  $\rightarrow$  Complete suspension



## PROBLEMATIC

Some industrial applications for solid-liquid mixing take place in the laminar regime which requires the use of more complicated impellers geometries like the Double Helical Ribbon (DHR) which generates complex flow, that implies new challenges for the modelisation.

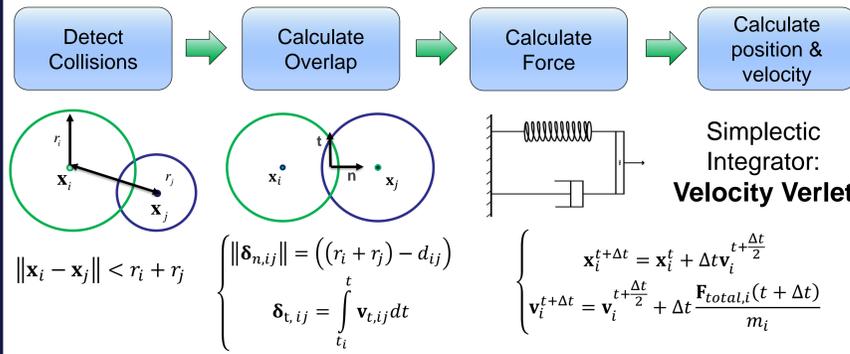


## OBJECTIVE

Develop a CFD-DEM in the rotational frame (Lagrangian frame) linked to the impeller in order to fix the CFD grid which offers plenty of new diverse applications.

## DISCRETE ELEMENT METHOD

Lagrangian approach where each particle is considered as a discrete entity in order to model granular flows



$$\mathbf{f}_{contact,ij} = -k_n \delta_{n,ij} - \gamma_n \mathbf{v}_{n,ij} - k_t \delta_{t,ij} - \gamma_t \mathbf{v}_{t,ij}$$

## EQUATIONS IN NON-INERTIAL FRAME

$$\frac{\partial \rho_f \epsilon_f \mathbf{u}}{\partial t} + \nabla \cdot (\rho_f \epsilon_f \mathbf{u} \otimes \mathbf{u}) = -\epsilon_f \nabla p + \nabla \cdot \boldsymbol{\tau} - \mathbf{f}_{pf} + \mathbf{f}_{inertial}$$

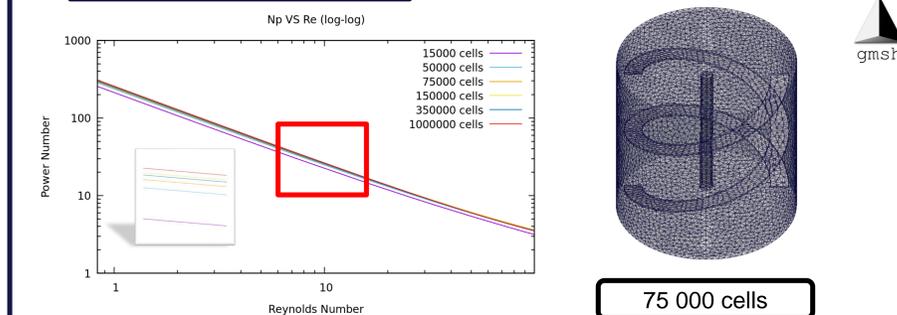
$$m_i \frac{d\mathbf{v}_i}{dt} = \sum_j \mathbf{f}_{c,ij} + \mathbf{f}_{p,ij} + \mathbf{f}_{inertial,i}$$

$$\mathbf{f}_{inertial} = \underbrace{\alpha \boldsymbol{\Omega} \times (\boldsymbol{\Omega} \times \mathbf{r})}_{Centrifugal} - \underbrace{2 \alpha \boldsymbol{\Omega} \times \mathbf{v}}_{Coriolis} + \alpha \mathbf{g} \quad \alpha \leftrightarrow \begin{cases} \rho_f \\ m_i \end{cases}$$

## METHODOLOGY

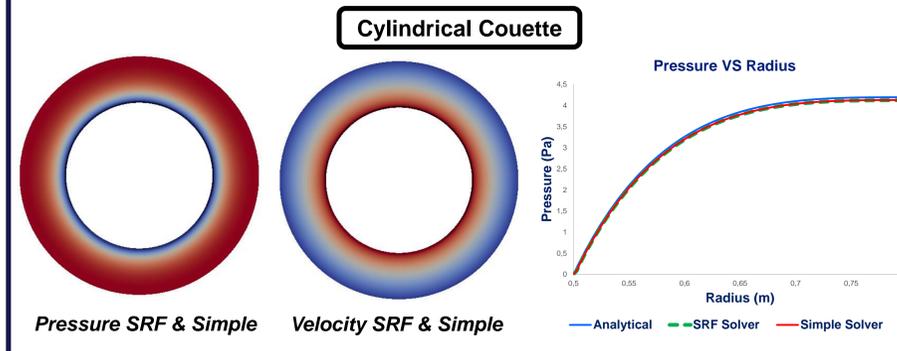
- Generate the mesh of the geometry with a convergence study
- Test the possibility to do DEM in non inertial frame
- Test the existing CFD solver for rotating frame
- Make a new PISO Solver for CFD-DEM in rotating frame
- Make a parameter study on viscosity, volume fraction of solid and density in order to understand the best use of Double Helical Ribbon

## MESH VALIDATION

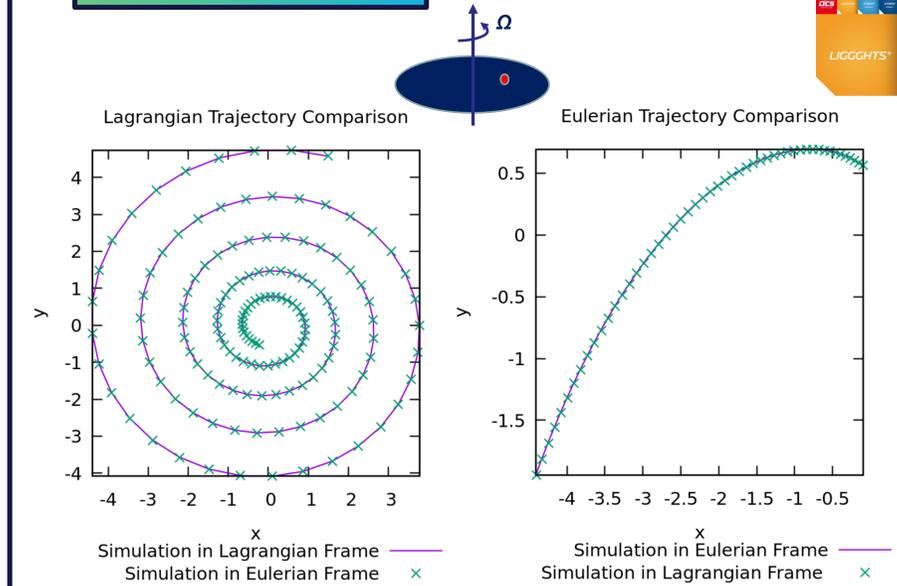


## CFD SOLVERS VALIDATION

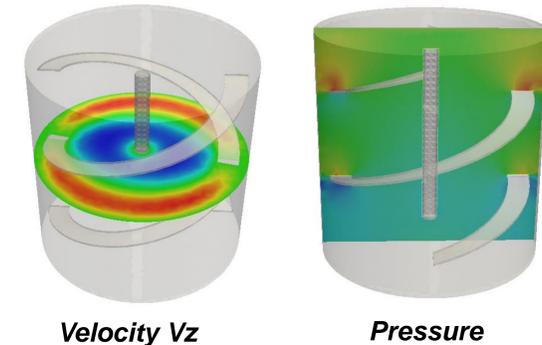
There are solvers in rotating frame in OpenFoam but we have to be sure of their implementation.



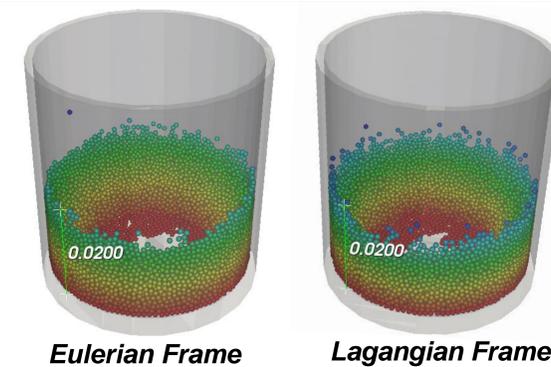
## DEM VERIFICATION



## PRELIMINARY RESULTS



**CFD**  
Pressure results without particles are coherent with experimental measurement

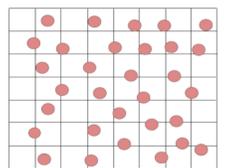


**DEM**  
Same height of particles in the two Frames

## CONCLUSIONS AND CFD-DEM APPROACH

All the preliminary results for the DEM and the CFD are conclusive  $\rightarrow$  GO TO CFD-DEM

**Unresolved CFD-DEM:**  
The fluid is solved at a scale coarser than particles  $\rightarrow$  Allow simulation with  $10^8$  particles



**Particles-Fluid Interaction:**  
Which forces should be taken into account?

- Drag Force
- Virtual Mass Force
- Basset Force
- Saffman Force
- Magnus Force

## NOMENCLATURE

- |   |   |
|---|---|
| <ul style="list-style-type: none"> <li><math>k_n</math>: Normal elastic coefficient</li> <li><math>k_t</math>: Tangential elastic coefficient</li> <li><math>\gamma_n</math>: Normal damp coefficient</li> <li><math>\gamma_t</math>: Tangential damp coefficient</li> <li><math>\delta_n</math>: Normal Overlap</li> <li><math>\delta_t</math>: Tangential Overlap</li> <li><math>\rho_f</math>: Liquid density</li> <li><math>\epsilon_f</math>: Void fraction</li> </ul> | <ul style="list-style-type: none"> <li><math>f_{c,ij}</math>: Contact force between particle i and j</li> <li><math>f_{pf,i}</math>: Interaction force between fluid and particle i</li> <li><math>\boldsymbol{\tau}</math>: Stress tensor</li> <li><math>\boldsymbol{\Omega}</math>: Rotation vector</li> <li>SRF: Single rotating Frame</li> <li>CFD: Computational Fluid Method</li> <li>DEM: Discrete Element Method</li> </ul> |
|---|---|

## ACKNOWLEDGMENTS

